

Finite time thermodynamics of a quantum dot heat engine



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Collaboration with

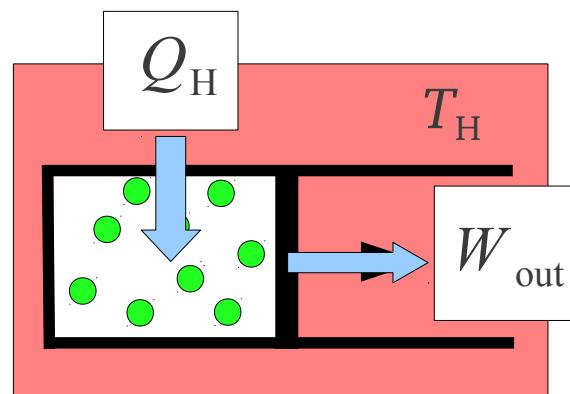


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(Hasselt)

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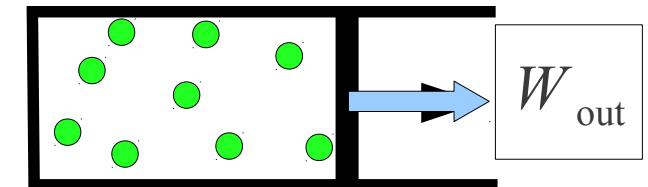
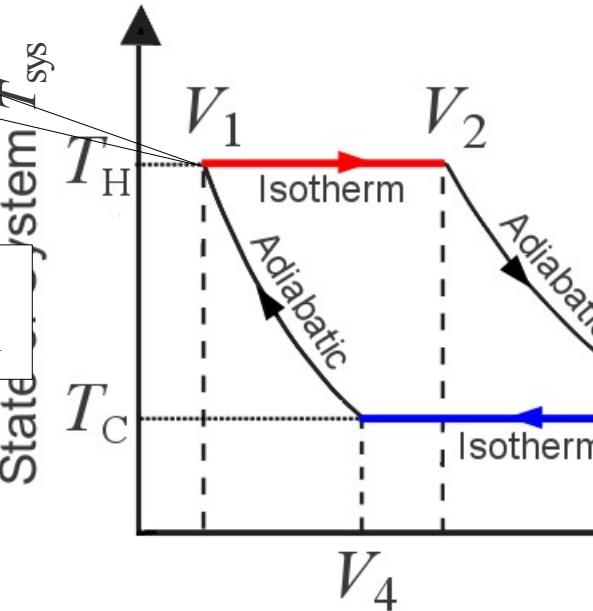
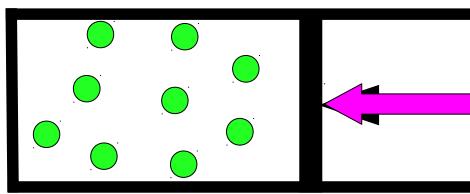
- Introduction
 - ◆ Carnot cycle and Carnot efficiency
 - ◆ Efficiency at maximum power and Curzon-Ahlborn efficiency.
- A case study: Quantum dot heat engine
- General derivation of the efficiency at maximum power with a weak dissipation approximation (model independent).
- Justification of the weak dissipation approximation for general Markovian processes.

Carnot Cycle



Sadi Carnot

Stop the piston when $T_{\text{sys}} = T_H$.

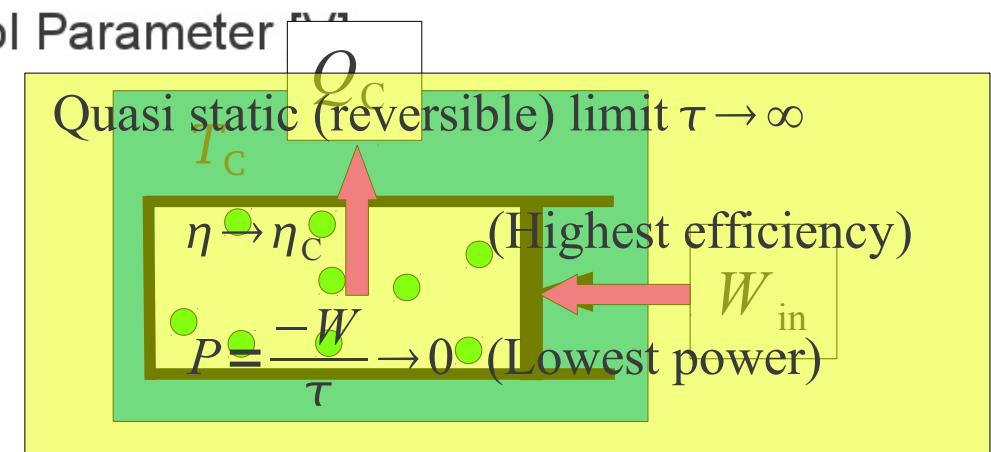


Stop the piston when $T_{\text{sys}} = T_C$.

Control Parameter

$$1\text{st Law: } W_{\text{Net}} + Q_H + Q_C = 0$$

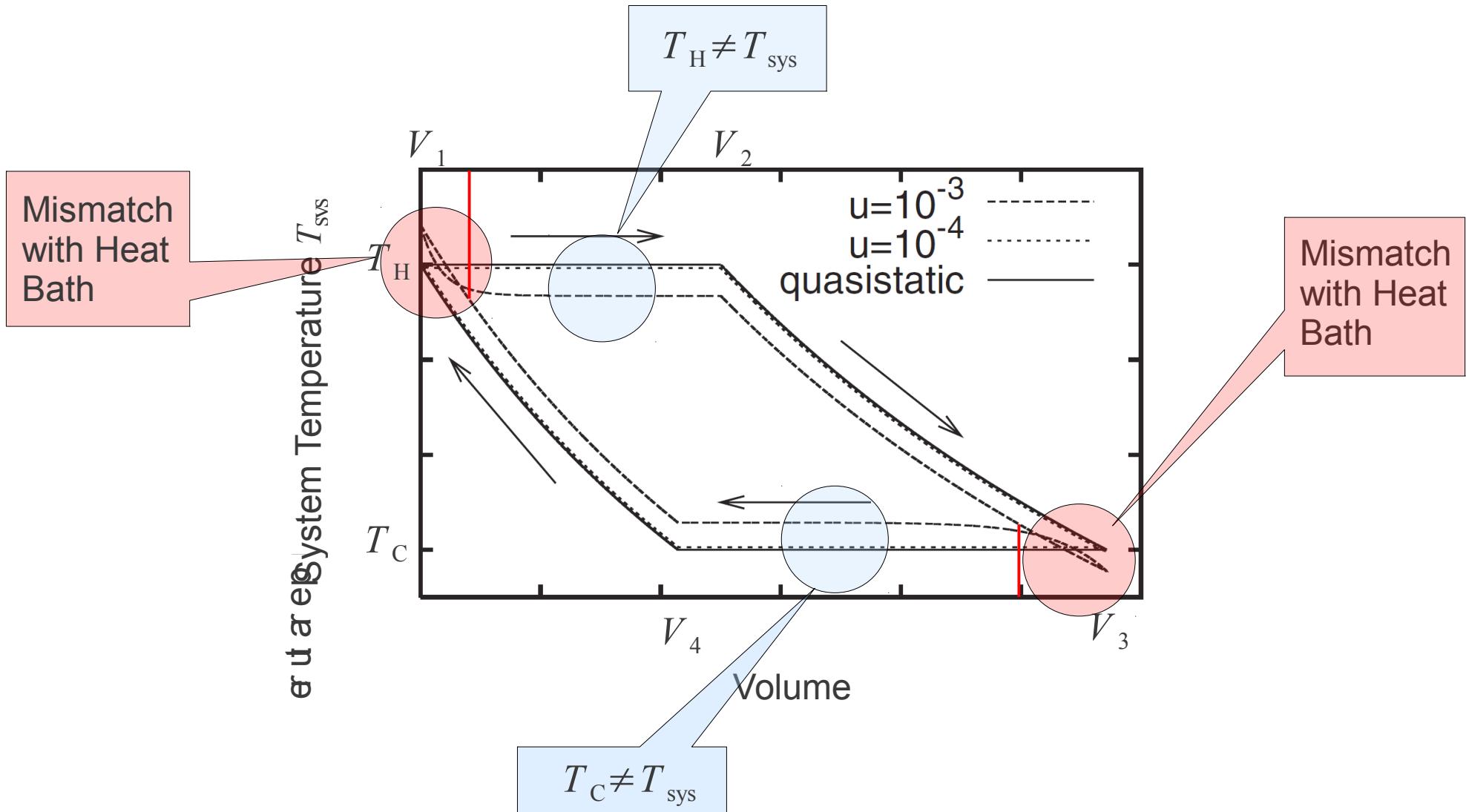
$$2\text{nd law: } \eta = \frac{-W_{\text{Net}}}{Q_H} = \leq 1 - \frac{T_C}{T_H} \equiv \eta_C$$



Finite Time Thermodynamics

Question: What will happen if τ is finite?

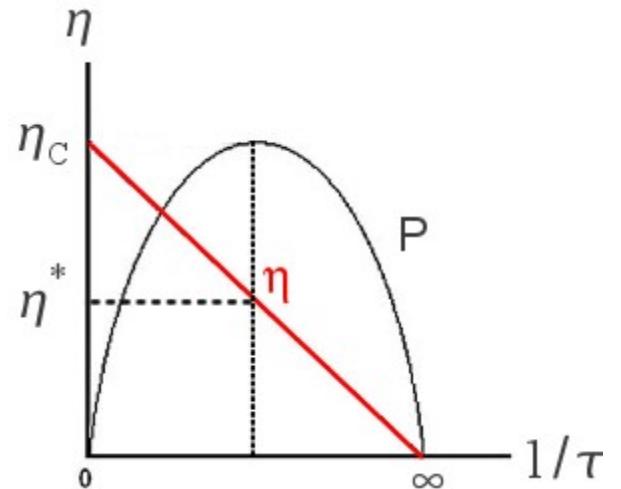
Textbook: The efficiency is lowered due to dissipation (entropy production).



Efficiency at maximum power

Efficiency decreases as τ increases.

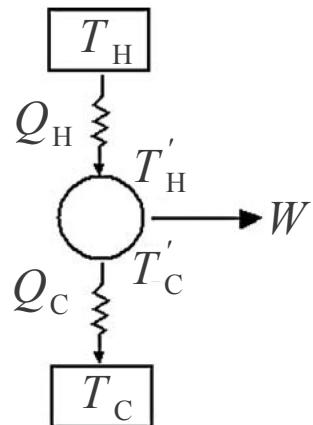
But Power reaches its maximum at a certain τ .



$$\text{maximum power: } P^* = \frac{-W}{\tau} = \frac{Q_H(\tau_H^*) + Q_C(\tau_C^*)}{\tau_H^* + \tau_C^*}$$

$$\text{efficiency at maximum power: } \eta^* = 1 + \frac{Q_C(\tau_C^*)}{Q_H(\tau_H^*)}$$

Curzon-Ahlborn efficiency



Efficiency at maximum power

$$\eta_{CA} = 1 - \sqrt{\frac{T_C}{T_H}}$$

Novikov, J. Nucl. Energy **II** (1958), 125

Curzon-Ahlborn, Am. J. Phys **43** (1975), 22

TABLE I. Observed performance of real heat engines.

Power source	T_C	T_H	η_C	η_{CA}	η_{Observed}
West Thurrock (U.K.) ² Coal Fired Steam Plant	~25	565	64.1%	40%	36%
CANDU (Canada) ⁴ PHW Nuclear Reactor	~25	300	48.0	28%	30%
Larderello (Italy) ⁵ Geothermal Steam Plant	80	250	32.3%	17.5%	16%
Steam power plant (USA)	298	923	67.6%	43.2%	40%

How universal is the Curzon-Ahlbone efficiency?

Many case studies:

$$\eta^* \approx \eta_{\text{CA}} = 1 - \sqrt{\frac{T_C}{T_H}} = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + \frac{\eta_C^3}{16} + \dots$$

Brownian heat engine [Schmiedl&Seifert, EPL **81** (2008), 20003]

$$\eta^* = \frac{2(T_H - T_C)}{3T_H + T_C} = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + \frac{\eta_C^3}{32} + \dots$$

Linear non-equilibrium thermodynamics

$$\eta^* = \frac{\eta_C}{2}$$

Van den Broeck, PRL **95** (2005), 190602

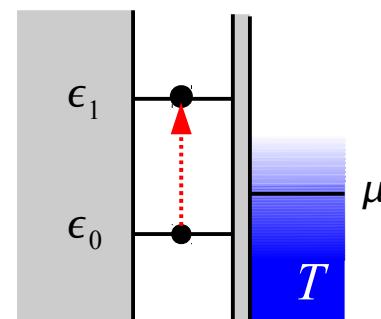
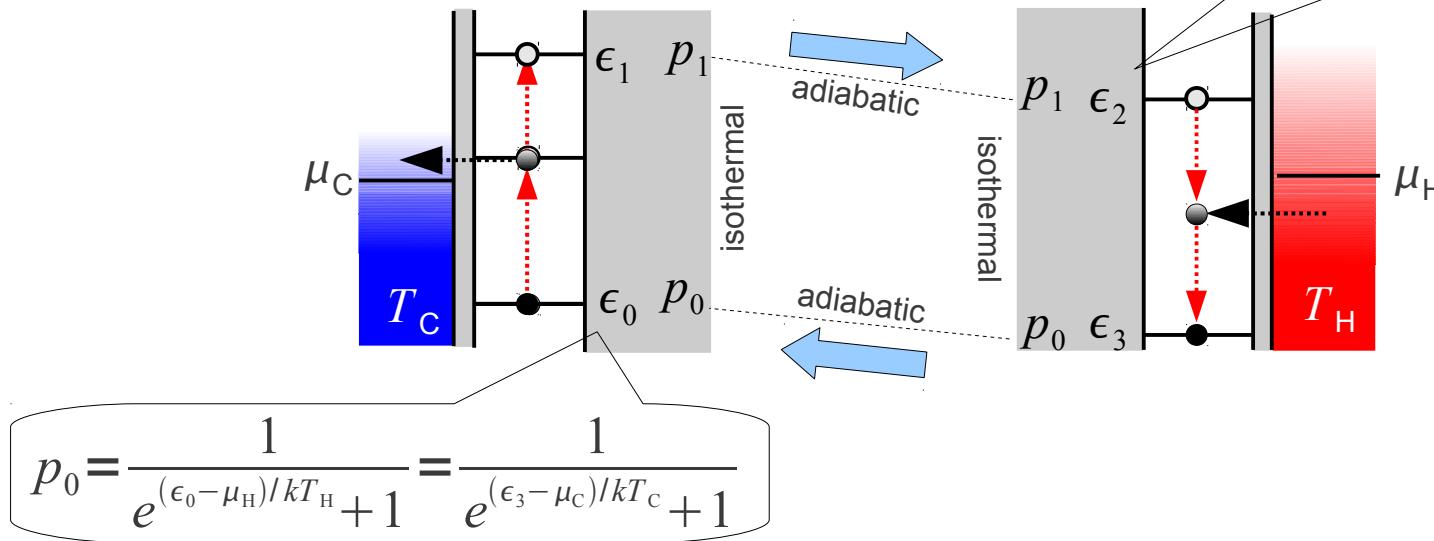
Non-linear correction (with left-right symmetry)

$$\eta^* = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + o(\eta_C^3)$$

Esposito *et al.*, PRL **102** (2009), 130602

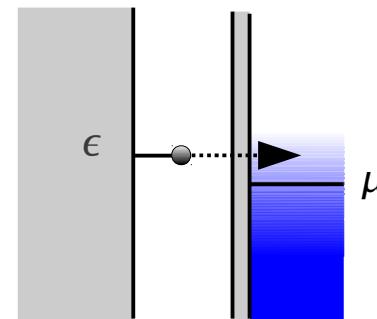
Quantum Dot Carnot Engine

Control parameter (protocol) $\epsilon(t)$



Work done to the system

$$W = \epsilon_1 - \epsilon_0$$



Heat flows out

$$Q = \epsilon - \mu$$

Steps to find efficiency at maximum power

Step 1: Find $\epsilon(t)$ that maximizes heat.

$$P = \frac{Q_H + Q_C}{\tau_H + \tau_C}$$

Step 2: Maximize power with respect to τ_H and τ_C

Step 3: Evaluate efficiency with optimum Q and τ

$$\eta = 1 + \frac{Q_C}{Q_H}$$

Master equation

$$\dot{p}(t) = -\omega_1 p(t) + \omega_2 [1 - p(t)] \implies \dot{p}(t) = -C p(t) + \frac{C}{e^{\epsilon(t)/kT} + 1}$$

$$\omega_1 = \frac{C}{e^{-\epsilon(t)/kT} + 1}, \quad \omega_2 = \frac{C}{e^{+\epsilon(t)/kT} + 1}$$

Work: $W[p(t)] = \int_0^\tau \dot{\epsilon}(t) p(t) dt$

Heat: $Q[p(t)] = \int_0^\tau \epsilon(t) \dot{p}(t) dt$

Step 1: Maximizing heat

$$Q[p(t)] = \int_0^\tau \epsilon(t) \dot{p}(t) dt = \int_0^\tau \ln\left[\frac{1}{C p(t) + \dot{p}(t)} - 1\right] \dot{p}(t) dt \equiv \int_0^\tau L(p, \dot{p}) dt$$

$$L(p, \dot{p}) = \ln\left[\frac{C}{C p(t) + \dot{p}(t)} - 1\right] \dot{p}(t)$$

$$\delta \int L dt = 0 \Rightarrow L - \dot{p} \frac{\partial L}{\partial \dot{p}} = \frac{\dot{p}^2}{(C p + \dot{p})(C(1-p) - \dot{p})} = K$$

K=1st integral of the motion

$$p(t) = \frac{1}{e^{\epsilon(t)/kT} + 1} \left[1 + \sqrt{K e^{\epsilon(t)/kT}} \right]$$

K measures the degree of dissipation.
The larger is K , the large is dissipation.

Carnot limit: $K \rightarrow 0$

Solution at Weak Dissipation Limit

$$K \ll 1$$

$$\Delta S_H = \Delta S_{rev} - \frac{[\phi_1 - \phi_0]^2}{C_H} \frac{1}{\tau_H}$$

$$\Delta S_C = -\Delta S_{rev} - \frac{[\phi_1 - \phi_0]^2}{C_C} \frac{1}{\tau_C}$$

$$\phi_i = \arcsin(1 - 2 p_i) \quad i=0,1$$

$$P = \frac{Q_H + Q_C}{\tau_H + \tau_C} = \frac{(T_H - T_C)\Delta S_{rev} - (\phi_1 - \phi_0)^2 \left[\frac{T_H}{C_H \tau_H} + \frac{T_C}{C_C \tau_C} \right]}{\tau_H + \tau_C}$$

$$\eta^* = 1 + \frac{Q_C^*}{Q_H^*} = \frac{\eta_C}{2} + \frac{\eta_C^2}{4 \left(1 + \sqrt{\frac{C_H}{C_C}} \right)} + \frac{\eta_C^3}{8 \left(1 + \sqrt{\frac{C_H}{C_C}} \right)} + \dots$$

$$\text{If } C_H = C_C \rightarrow \eta^* = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + \frac{\eta_C^3}{16} + \dots = \eta_{CA}$$

Generalization

$$\Delta S = \Delta S^e + \Delta S^i$$

Change in system entropy

Internal entropy production

Entropy flow: $\Delta S^e = \frac{Q}{T}$

Quasi static limit $\tau \rightarrow \infty$: $\Delta S^e \rightarrow \Delta S^{\text{rev}}$, $\Delta S^i \rightarrow 0$

Asymptotic expansion (Weak dissipation approximation)

$$\Delta S^e = \Delta S^{\text{rev}} - \frac{\Sigma^e}{\tau} + o\left(\frac{1}{\tau^2}\right)$$

$$\Delta S^i = \frac{\Sigma^i}{\tau} + o\left(\frac{1}{\tau^2}\right)$$

Heat

$$Q_H = T_H \Delta S_H^e \approx T_H \Delta S^{\text{rev}} - \frac{T_H \Sigma_H^e}{\tau_H}$$
$$Q_C = T_C \Delta S_C^e \approx -T_C \Delta S^{\text{rev}} - \frac{T_C \Sigma_C^e}{\tau_C}$$

Power

$$P = \frac{Q_H + Q_C}{\tau_H + \tau_C} = \frac{(T_H - T_C) \Delta S^{\text{rev}} - \frac{T_H \Sigma_H^e}{\tau_H} - \frac{T_C \Sigma_C^e}{\tau_C}}{\tau_H + \tau_C}$$

Maximizing power with respect to τ_H and τ_C

$$\tau_H^* = \frac{2 T_H \Sigma_H^e}{(T_H - T_C) \Delta S^{\text{rev}}} \left(1 + \sqrt{\frac{T_C \Sigma_C^e}{T_H \Sigma_H^e}} \right)$$

$$\tau_C^* = \frac{2 T_C \Sigma_C^e}{(T_H - T_C) \Delta S^{\text{rev}}} \left(1 + \sqrt{\frac{T_H \Sigma_H^e}{T_C \Sigma_C^e}} \right)$$

Efficiency at *Maximum Power*

$$\eta^* = 1 + \frac{Q_C^*}{Q_H^*} = \frac{\eta_C}{2} + \frac{\eta_C^2}{4 \left(1 + \sqrt{\frac{\sum_e}{\sum_H}} \right)} + \frac{\eta_C^3}{8 \left(1 + \sqrt{\frac{\sum_e}{\sum_H}} \right)} + \dots$$

$$\frac{\sum_e}{\sum_H} = \infty \rightarrow \eta^* = \frac{\eta_C}{2}$$

$$\frac{\sum_e}{\sum_H} = 0 \rightarrow \eta^* = \frac{\eta_C}{2} + \frac{\eta_C^2}{4} + \frac{\eta_C^3}{8} + \dots = \frac{\eta_C}{2 - \eta_C}$$

$$\frac{\sum_e}{\sum_H} = 1 \rightarrow \eta^* = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + \frac{\eta_C^3}{16} + \dots = \eta_{CA}$$

$$\frac{\eta_C}{2} \leq \eta^* \leq \frac{\eta_C}{2 - \eta_C}$$

η_{CA}

Exactly in the middle
of two bounds



I think I have already
said so.

Schmiedl & Seifert (2008)

TABLE I. Observed performance of real heat engines.

Power source	T_C	T_H	η_C	η_{CA}	η_{Observed}	Lower bound	Upper bound
West Thurrock (U.K.) ² Coal Fired Steam Plant	~25	565	64.1%	40%	36%	32%	47%
CANDU (Canada) ⁴ PHW Nuclear Reactor	~25	300	48.0	28%	30%	24%	31%
Larderello (Italy) ⁵ Geothermal Steam Plant	80	250	32.3%	17.5%	16%	16%	19%
Steam power plant (USA)	298	923	67.6%	43.2%	40%	34%	51%

Justification of asymptotic expansion

An isothermal process: a master equation

$$\dot{P}_m(t) = \sum_n W_{mn}^T(t) P_n(t)$$

$$W_{mn}^T(t) = W_{mn}^T[\lambda(t/\tau)]$$

$$\sum_m W_{mn}^T(t) = 0$$

Scaling time

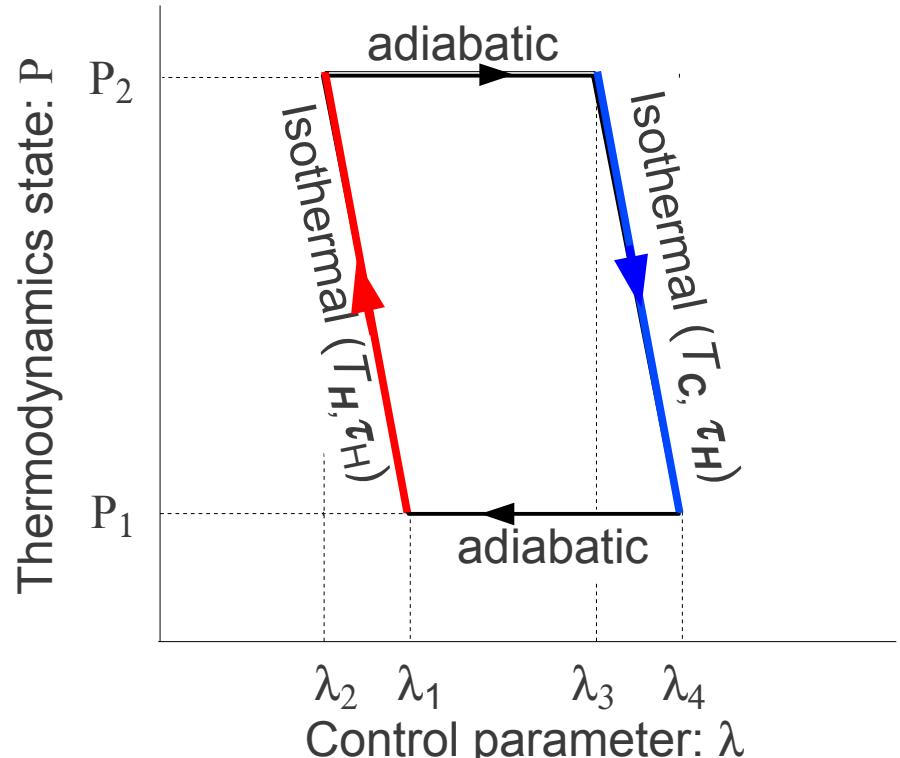
$$\frac{d}{ds} |P_\tau(s)\rangle = \tau \hat{W}^T(s) |P_\tau(s)\rangle \quad s = \frac{t}{\tau}$$

Asymptotic expansion

$$|P_\tau(s)\rangle = |P^{\text{st}}(s)\rangle + \frac{1}{\tau} |\delta^{(1)}(s)\rangle + \frac{1}{\tau^2} |\delta^{(2)}(s)\rangle + o\left(\frac{1}{\tau^3}\right)$$

$$\hat{W}^T(s) |P^{\text{st}}(s)\rangle = 0, \text{ Detailed balance} \quad W_{mn}^T(s) P_n^{\text{st}}(s) = W_{nm}^T(s) P_m^{\text{st}}(s)$$

$$\hat{W}^T(s) |\delta^{(1)}(s)\rangle = \frac{d}{ds} |P^{\text{st}}(s)\rangle, \quad \hat{W}^T(s) |\delta^{(2)}(s)\rangle = \frac{d}{ds} |\delta^{(1)}(s)\rangle \quad \sum_m \delta_m^{(1)} = \sum_m \delta_m^{(2)} = 0$$



Entropy flow

$$\begin{aligned}\Delta S^e &= \int_0^\tau dt \sum_m \sum_n W_{mn}(t) P_n(t) \ln \left[\frac{W_{nm}(t)}{W_{mn}(t)} \right] \\ &= \Delta S^{\text{rev}} - \frac{1}{\tau} \int_0^1 ds \sum_m \left[\frac{d}{ds} \delta_m^{(1)}(s) \right] \ln P_m^{\text{st}}(s)\end{aligned}$$

$$\Delta S^{\text{rev}} = -k \sum_m P_m^{\text{st}}(\tau) \ln P_m^{\text{st}}(\tau) + k \sum_m P_m^{\text{st}}(0) \ln P_m^{\text{st}}(0)$$

Entropy production

$$\begin{aligned}\Delta S^i &= \int_0^\tau dt \sum_m \sum_n W_{mn}(t) P_n(t) \ln \left[\frac{W_{mn}(t) P_n(t)}{W_{nm}(t) P_m(t)} \right] \\ &= -\frac{1}{\tau} \int_0^1 ds \sum_m \delta_m^{(1)}(s) \left[\frac{d}{ds} \ln P_m^{\text{st}}(s) \right]\end{aligned}$$

Conclusions

- 1) The efficiency at maximum power is derived without a specific model at the weak dissipation limit, .
- 2) The minimum efficiency at maximum power is $\eta_C/2$. (If only dissipation due to finite time is taken into account.)
- 3) The maximum efficiency at maximum power is $\eta_C/(2-\eta_C)$
- 4) Exact Curzon-Ahlborn efficiency is obtained when left-right symmetry holds and it lies right in the middle between the lower and upper bounds.
- 5) Only maximization of power with respect to operation times is necessary to get the Curzon-Ahlborn efficiency
- 6) The method of asymptotic expansion (weak dissipation limit) is justified for general Markovian processes.
- 7) The general results are demonstrated using analytically solvable model based on a quantum dot Carnot engine.

Determination of K

$$C_\alpha \tau_\alpha = F(p(\tau_\alpha), K) - F(p(0), K)$$

$$F(p, K) = \frac{-1}{2} \ln p + \frac{1}{\sqrt{K}} \arctan \left[\frac{1-2p}{\sqrt{K+4p(1-p)}} \right] + \frac{1}{2} \ln \left[\frac{2p+K+\sqrt{K^2+4p(1-p)}}{2(1-p)+K+\sqrt{K^2+4Kp(1-p)}} \right]$$

Exact Entropy flow

$$Q = T \Delta S^e = \mathcal{S}(p(\tau), K) - \mathcal{S}(p(0), K)$$

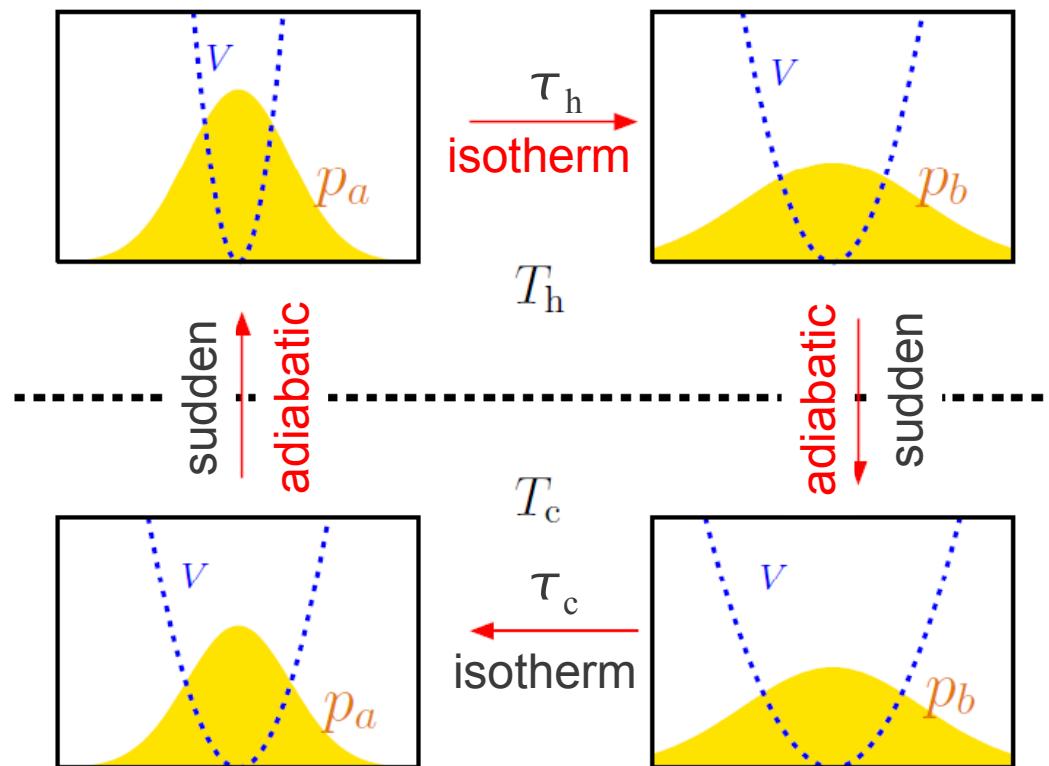
$$\mathcal{S}(p, K) = p \ln \left[\frac{2(1-p)p+K-\sqrt{K^2+4Kp(1-p)}}{2p^2} \right] - \sqrt{K} \arcsin \left[\frac{1-2p}{\sqrt{K+1}} \right] - \ln \left[\frac{2(1-p)-K-\sqrt{K^2+4Kp(1-p)}}{2} \right]$$

Protcols

$$p_C(t) = \frac{1}{2} \left[1 - \sin \left(\frac{t}{\tau_C} |\phi_1 - \phi_0| + \phi_0 \right) \right]$$

$$p_H(t) = \frac{1}{2} \left[1 + \sin \left(\frac{t}{\tau_H} |\phi_1 - \phi_0| - \phi_1 \right) \right]$$

Brownian heat engine



Controle parameter: spring constant

Thermodynamic state: density $p(x)$

$$\eta^* = \frac{2(T_h - T_c)}{3T_h + T_c} = \frac{\eta_C}{2} + \frac{\eta_C^2}{8} + \frac{\eta_C^3}{32} + \dots$$